



# Scaling-up from High Throughput Screening to Continuous Process for the Synthesis of 1,6-Hexanediol from Renewable Feedstocks

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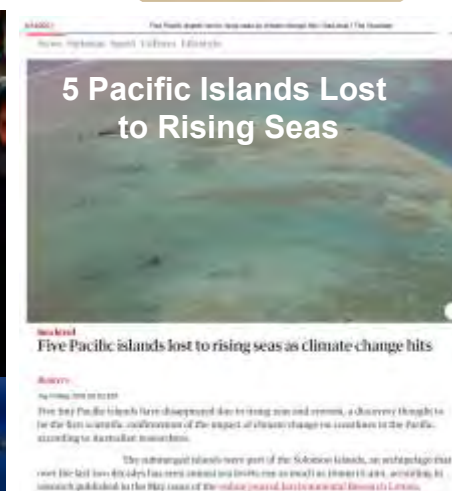
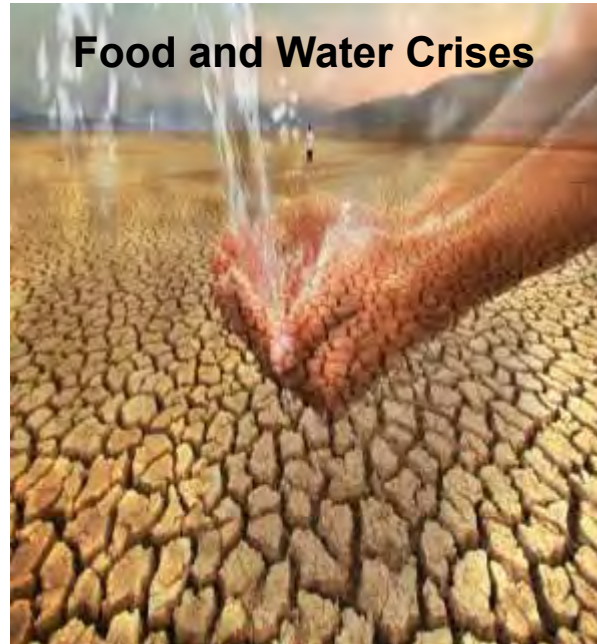


# Outline

- **Overview**
  - Effect of Climate Change
  - Sustainable Development
- **Biomass to Value Added Monomers**
  - Objectives
  - Approach
- **Renewable Monomers via Selective Hydrodeoxygenation**
  - Diols from Carbohydrate Feedstock
- **Catalyst Synthesis and Selection**
  - Catalyst Synthesis and Characterization
- **Catalyst Evaluation**
  - High Throughput Catalyst Synthesis & Screening
  - Scale up in Continuous Fixed Bed Reactors
- **Summary**



# Environmental Crisis and Sustainable Development





Naomi Klein

*“Climate change isn’t an ‘issue’ to add to the list of things to worry about ... it’s a civilizational wake-up call ... telling us that we need an entirely new economic model”*



Alexa Dembek

*“We need to decouple carbon from growth”*

# DuPont's Ten-year Path to a More Sustainable Future



innovate **now**

**Delivering solutions for global challenges**

Align 100% of the DuPont innovation portfolio to meaningfully advance the UN SDGs and create value for our customers



protect **now**

**Acting on climate**

Reduce Green House Gas (GHGs) emissions 30% including sourcing 60% of electricity from renewable energy



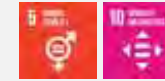
Deliver carbon neutral operations by 2050



empower **now**

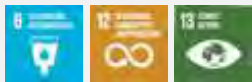
**Accelerating diversity, equity & inclusion**

Become one of the world's most inclusive companies, with diversity well ahead of industry benchmarks



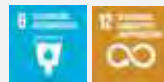
**Enabling a circular economy**

Integrate circular economy principles into our business models considering lifecycle impacts in the markets we serve



**Leading water stewardship**

Implement holistic water strategies across all facilities prioritizing manufacturing plants and communities in high-risk watersheds



Enable millions of people access to clean water through leadership in advancing water technology and enacting strategic partnerships

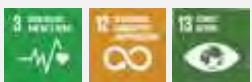
**Cultivating well-being & fulfillment**

Create a workplace where employees report high levels of well-being and fulfillment



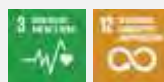
**Innovating safer by design**

Design 100% of our products and processes using sustainability criteria including the principles of green chemistry



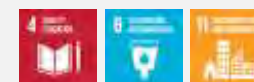
**Delivering world-class health & Safety**

Further our commitment to zero: injuries, occupational illnesses, and incidents



**Building thriving communities**

Improve over 100 million lives through targeted social impact programs





# Objectives

- **High value monomer production from bio-renewable resources**
  - Design and develop cost-advantaged, inherently safe, and sustainable processes based on renewably-sourced feedstocks for the production of fuels, chemicals, and advanced materials
- **Selective hydrodeoxygenation (HDO) of biomass-derived feedstocks**
  - Develop a cost-competitive process for the synthesis of 1,6-hexanediol from renewable feedstocks
  - Determine the activity, selectivity, and life of supported metal-metal oxide catalyst combinations using high throughput screening and continuous trickle bed reactors for the hydrodeoxygenation of 1,2,6-hexanetriol (1,2,6-HT) and tetrahydropyran-2-methanol (THP2M) to 1,6-hexanediol (1,6-HD)

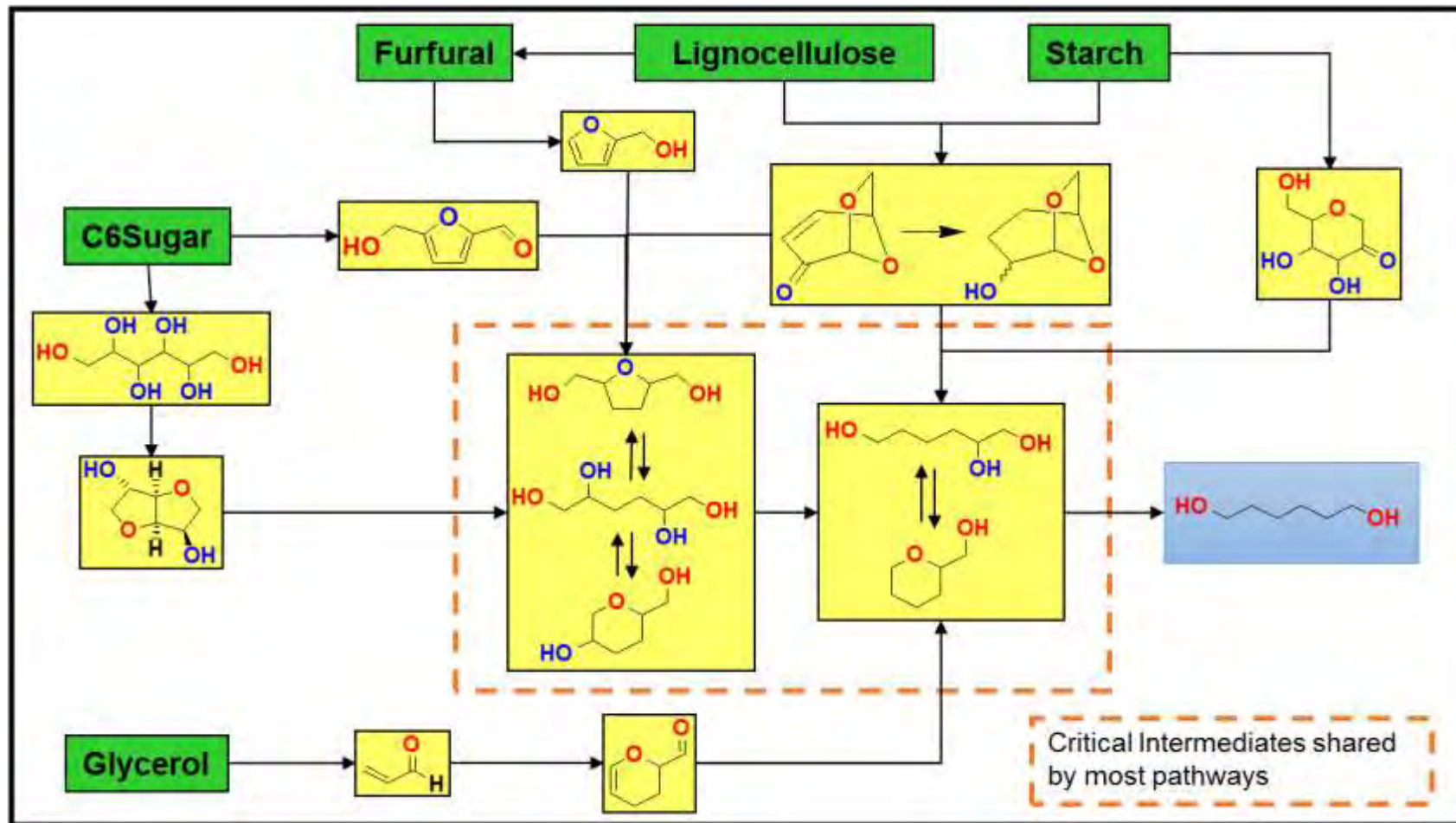
# Industrially Important Polyols from Biomass

**Opportunity:** Conversion of inexpensive oxygen-rich biomass into industrially useful functionalized building blocks

Biomass		Diol	Application
<b>Glycerol</b> waste by-product of biodiesel production	<chem>OCC(O)CO</chem>	<chem>OCCCO</chem> <b>1,3-Propanediol</b>	Sorona™ (DuPont) Corterra™ (Shell)
<b>Erythritol</b> Biofermentation of cornsugar/starch	<chem>OCC(O)C(O)CO</chem>	<chem>C1CCOC1</chem> <b>THF</b>	Lycra™ Industrial Solvent
<b>Xylitol</b> Acid digestion/pyrolysis hemi-cellulose eg: corn cobs	<chem>OCC(O)C(O)C(O)CO</chem>	<chem>OCCCCCO</chem> <b>1,5-Pentanediol</b>	Thermoplastic Polyurethanes Polyesters
<b>Sorbitol</b> hydrogenation of glucose from corn/beet/cane sugar	<chem>OCC(O)C(O)C(O)C(O)CO</chem>	<chem>OCCCCCCO</chem> <b>1,6-Hexanediol</b>	Polyurethanes Polyesters Potential Nylon-6,6 precursor

Fluctuations in oil prices and increase in greenhouse gas emission have prompted the quest for alternative cost-competitive pathways for the synthesis of chemicals, materials, and fuel from renewable feedstocks

# Conversion of Biomass to Renewable 1,6-HD



Reaction network delineating key intermediates for converting various biomass to renewable 1,6-hexanediol (1,6-HD)



# Process Development, Design, and Scale-up

## *Lab, Pilot, and Commercial Scale Reactors*

Lab Scale Reactor	Pilot Scale Reactor	Commercial Scale Reactor
Design for basic data	Design to confirm commercial reactor concept	Design reaction condition for optimal performance
Scale up or scale down of commercial reactor	Scale down of commercial scale reactor, as close as possible	Safe, low footprint, minimal upstream and downstream processing
Maintain isothermal condition	May require more than one scale	Model required to evaluate optimal conditions
Model required for interpretation of data	Iterate between lab and pilot to refine design and operating conditions	Iterate with lab and pilot scale reactors to refine design and operating conditions

# Batch vs Continuous Processes

Batch Process	Continuous Process
Can be easily adapted to different processes/chemistries (tolling)	Higher throughput
Well-suited for small scale operation (specialty chemicals)	Benefit of scale
Suitable for complex recipes (e.g. pharma, biotech)	Higher uptime
Well mixed system	Lower inventory of feed/product in reactor
Near isothermal condition	Easy coupling with continuous upstream and downstream processes
Higher mass and heat transfer	Higher yield/selectivity
Easy scale-up and scale-down	Better safety, control and operability, lower environmental footprint
Easy to operate	Lower capital investment

# hte

## *The High Throughput Experimentation Company*



- Turn-key ready test systems
  - Contract research
- for catalyst R&D



Client owns IP on  
catalyst and  
process




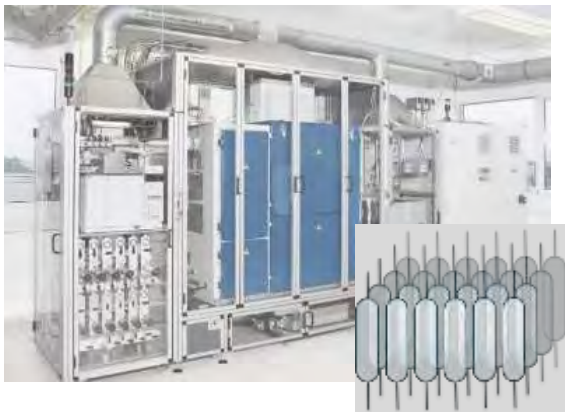


Fields of  
competencies





# Overview of hte Toolbox

## *Development from Batch to Continuous Flow Reactors*

Batch	fixed bed		fluidized bed
 <p>Batch / semi-batch reactors (x8 fold)</p>	 <p>Gas phase &amp; trickle-bed reactors (x16 – x48 fold) powder and extrudate</p>	 <p>Bench-scale system (x1 - x8 fold) extrudate</p>	 <p>Micro Down-Flow Unit (MDU)</p>
<ul style="list-style-type: none"><li>• Catalyst testing</li><li>• Feed testing</li><li>• POCs</li></ul>	<ul style="list-style-type: none"><li>• Catalyst testing</li><li>• Feed screening</li><li>• ~1-50 ml of catalyst</li></ul>	<ul style="list-style-type: none"><li>• Process optimization</li><li>• Upscaling</li><li>• ~100 – 300 ml of catalyst</li></ul>	<ul style="list-style-type: none"><li>• Fluidized bed catalyst testing</li></ul>



8-15

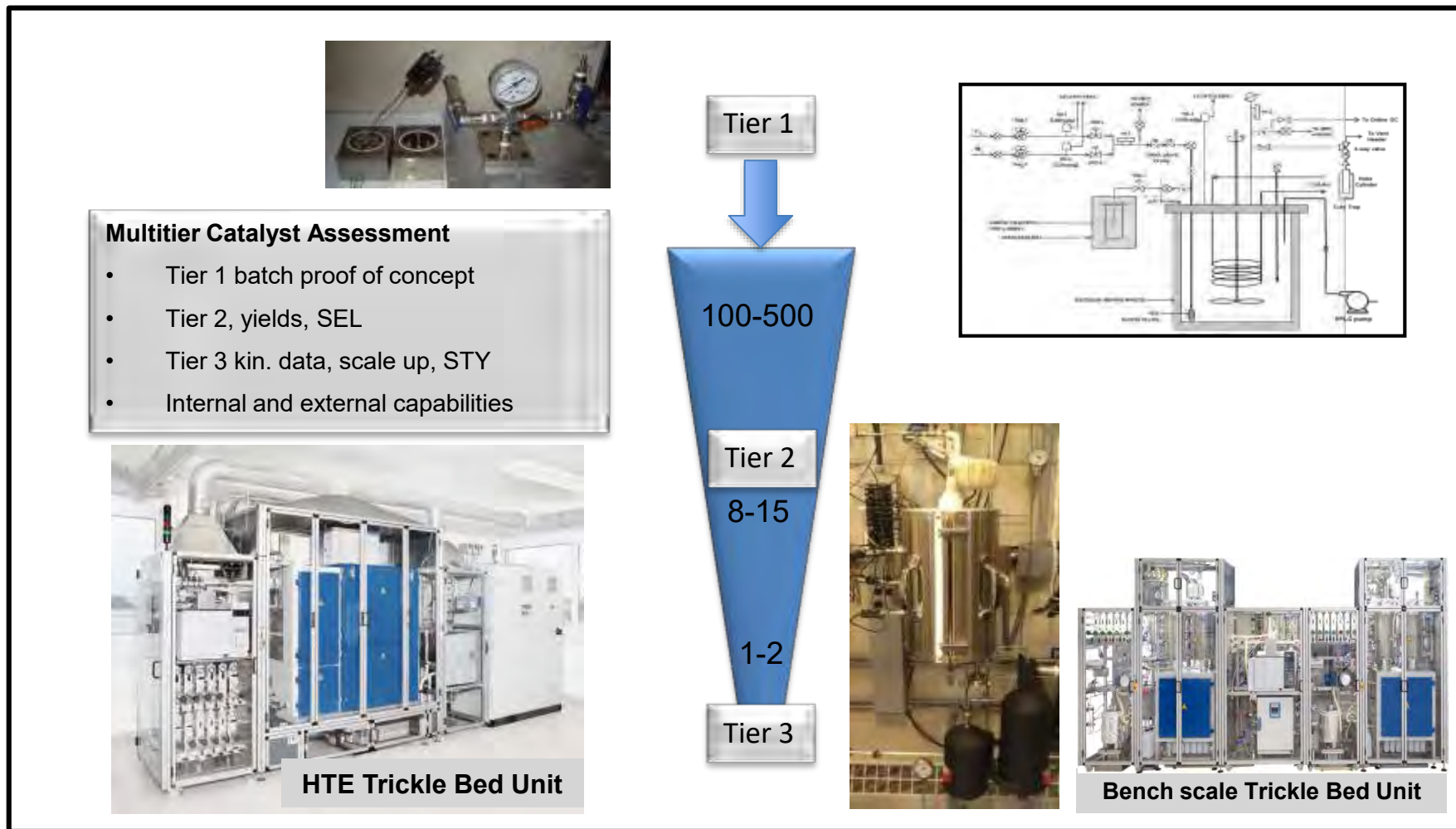
### Tier 3

- Tier 1, powder synthesis – incipient wetness impregnation, co-precipitation
- Tier 2, upscaling – shell impregnation
- Tier 3, lead optimization (loading, support)



**DUPONT**

# Catalyst Testing Tool Box



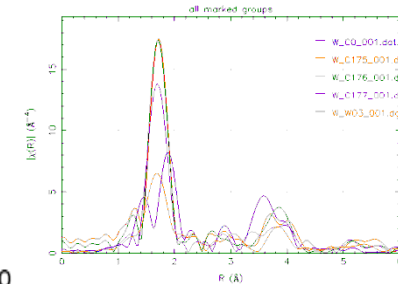
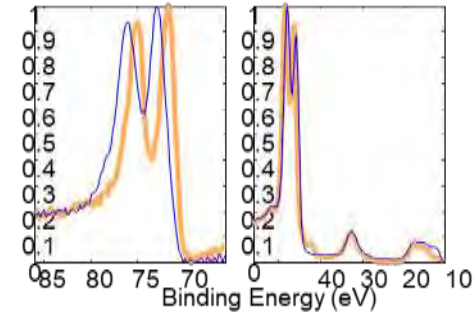
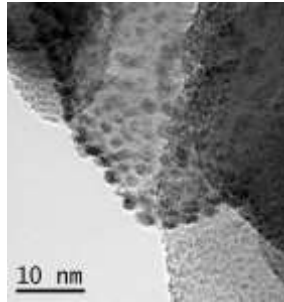
Multitier catalyst screening strategy was used, internally and externally, to determine lead catalyst candidates and subsequent process development and catalyst optimization



# Analytical Tool Box

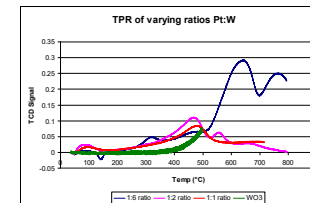
## Catalyst characterization

- BET, PVD, PSD
- TG, Chemisorption, TPD
- Density, Strength
- XRD, XRF, XAS
- ESCA
- TEM, SEM, EDS
- EA, ICP-OES/MS



## Offline GC for product characterization

- Method development
- Optimization of given method (e.g. run length 2 h → 1 h)



## Compound identification – GC-MS & Injection

- Varying substrates & solvents
- Approx. 180 compounds identified – known & unknown

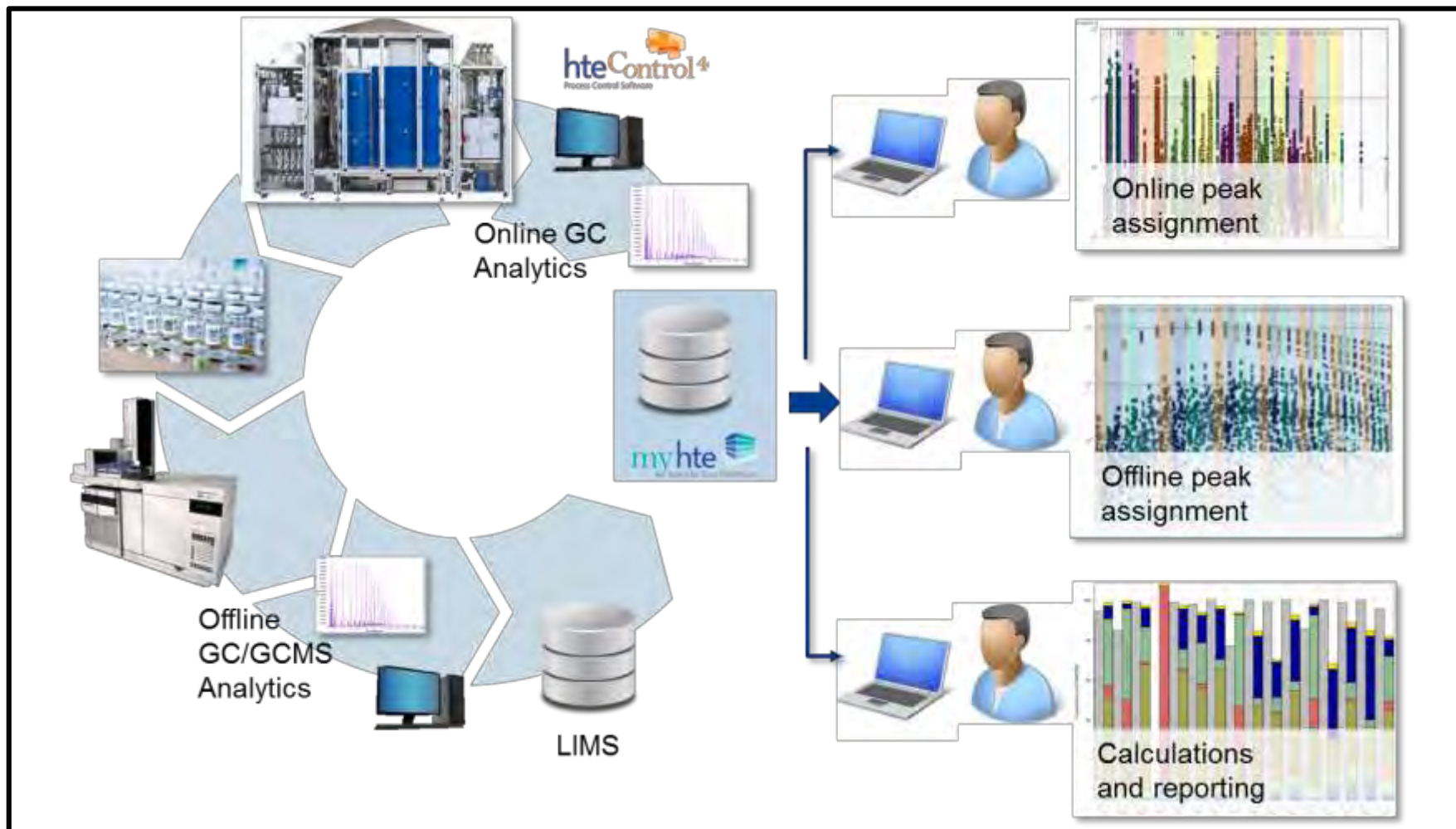
## Peak separation and quantification

- Proper peak separation and high sample throughput
- Two Agilent GC 7890 Dual Channel 2xFID in operation



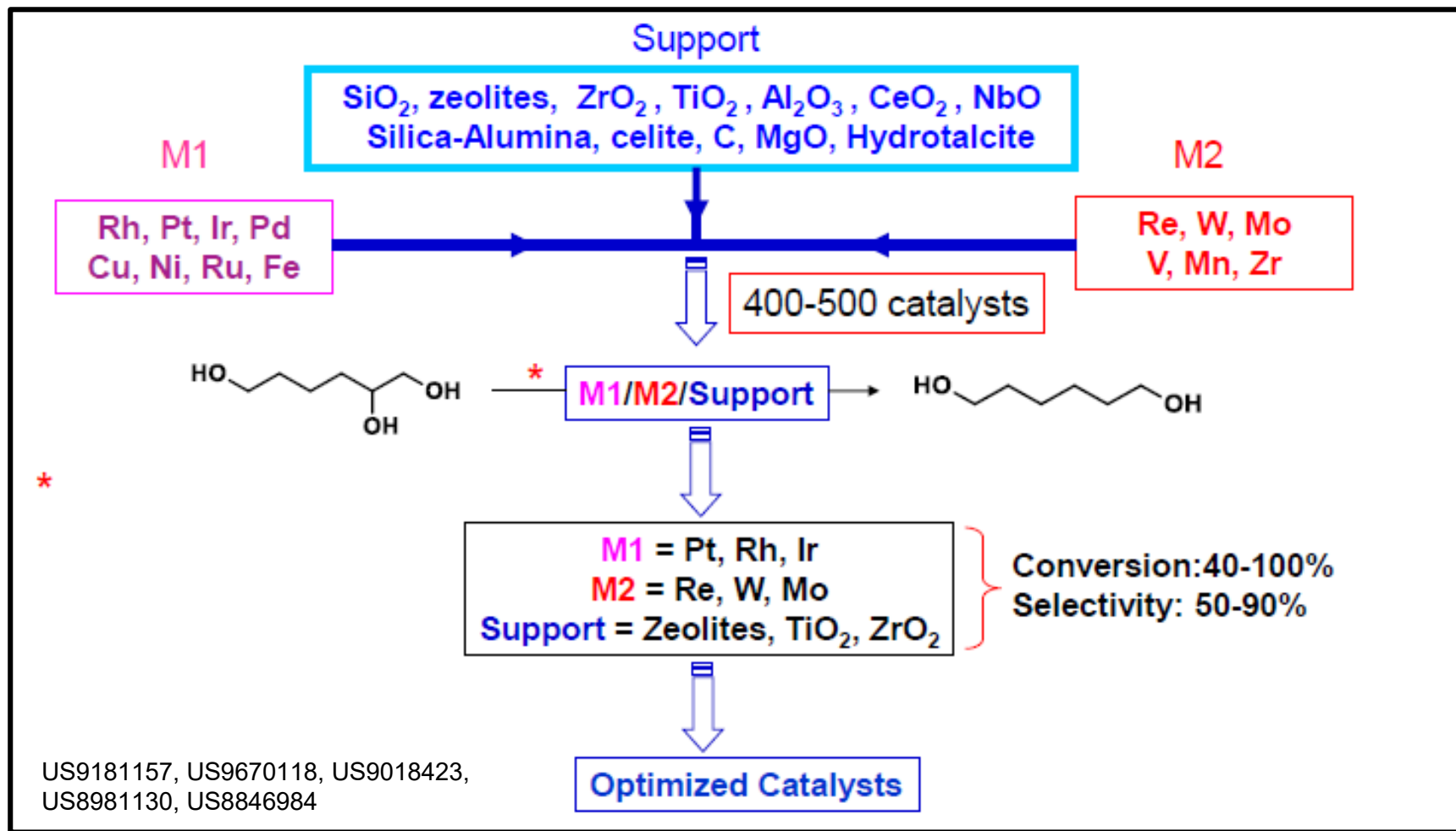
Detailed characterization of catalyst, feedstocks, and gaseous and liquid products by various analytical tools to optimize catalysts and quantify product distribution as a function of catalyst and feedstock

# Data Collection and Integration Tool Box



Integrated software workflow for collecting, evaluating and reporting all operational, gas and liquid samples as well as, kinetic data in a comprehensive database

# Catalyst Synthesis



Plethora of reducible metal and oxophilic metal oxide combinations were prepared and tested in high-throughput catalyst screening reactors for catalyst evaluation



# Catalyst Upscaling

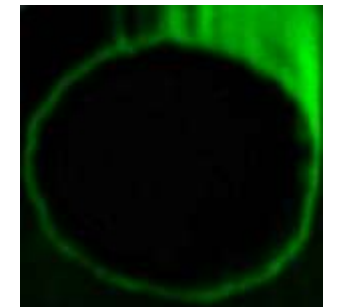
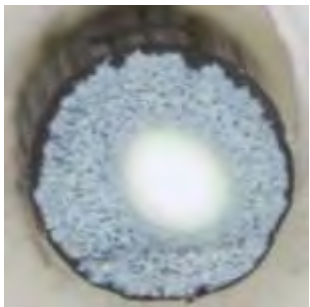
## *From Powder to Extrudate*



Shell Impregnation

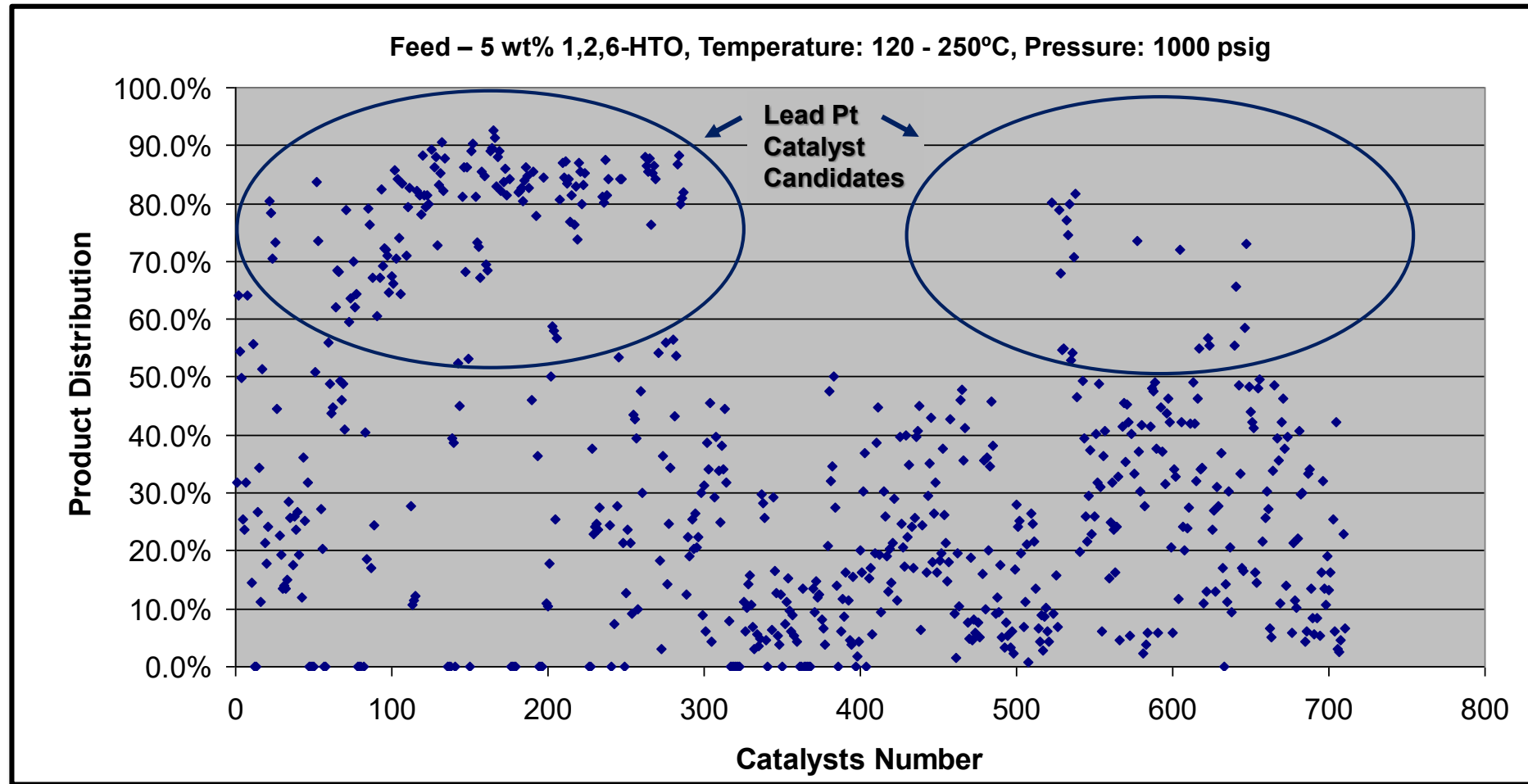


Full characterization of the synthesized catalysts by different techniques:  
BET, PVD, PSD, TG, Density, Strength, XRD, XRF, EA, ICP-OES/MS  
Shell thickness optimization and investigation of metal loading vs catalytic activity



Shell thickness measurement using microscopic techniques

# Catalyst Screening



Identified catalyst compositions and synthesis techniques to achieve single pass >70 mol% 1,6-HD.

# Trickle Bed Reactor Test Units



Catalyst embedding



16-fold high-throughput trickle-bed reactor unit

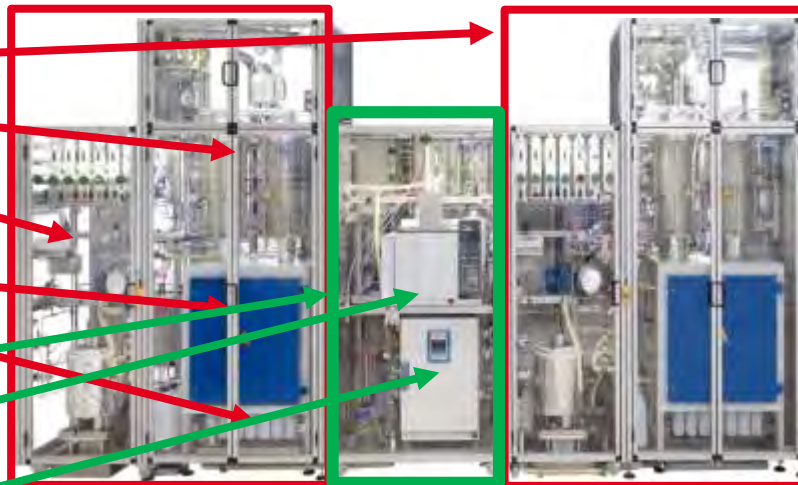
- Cover all trickle bed applications
- Simulating industrial operating conditions
  - Up to 450°C (higher on-demand)
  - 4x4 heating blocks or 16 individual heaters
  - Up to 260 barg
  - Up- or downflow, once-through, reactors in series, interstage dosing/sampling, adiabatic T-profile
- Reactor: ID 5 – 8 mm, up to 200 mm isothermal zone
- Catalyst: up to 10 ml, powder, commercial shapes
- One or two liquid feed supplies
- Full mass balance of gas and liquid products
- Automated 24/7 operation

## Independent Modules

- 2 reactors (parallel/series)
- Gas/liquid supply
- Downstream Separator
- Liquid sampling

## Analytics

- Online GC
- Heating/Valves, FI – Gas flow



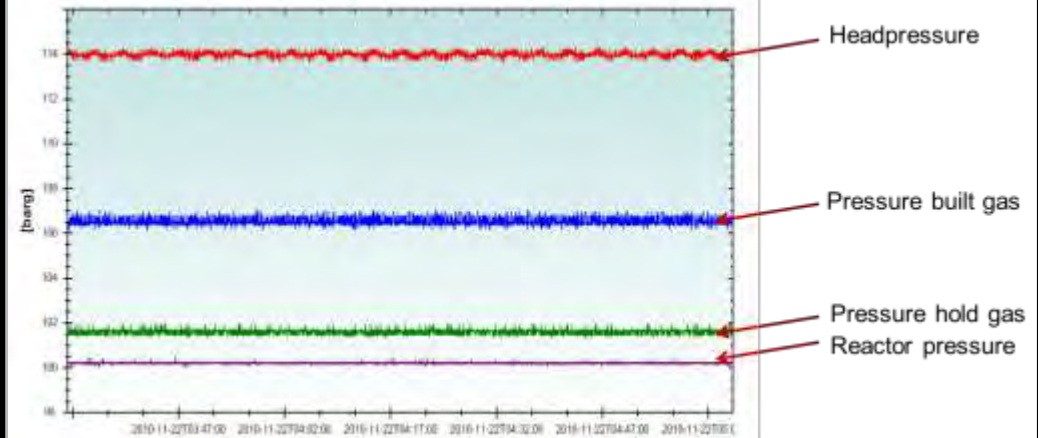
8-fold bench-scale trickle-bed reactor unit

- Cover all trickle bed applications
- Simulating industrial operation conditions
  - Up to 450°C (higher on-demand), individual heaters
  - Up to 170 barg (higher on-demand)
  - Up-/downflow, once-through, reactors in series, interstage dosing/sampling, adiabatic T-profiles
- Reactor: ID 12 – 24 mm, up to 300 mm isothermal zone
- Catalyst: up to 80 ml, commercial shapes
- Individual operation with separate feed and operating variables per module (4 modules with 2 reactors each)
- Full mass balance of gas and liquid products
- Automated 24/7 operation

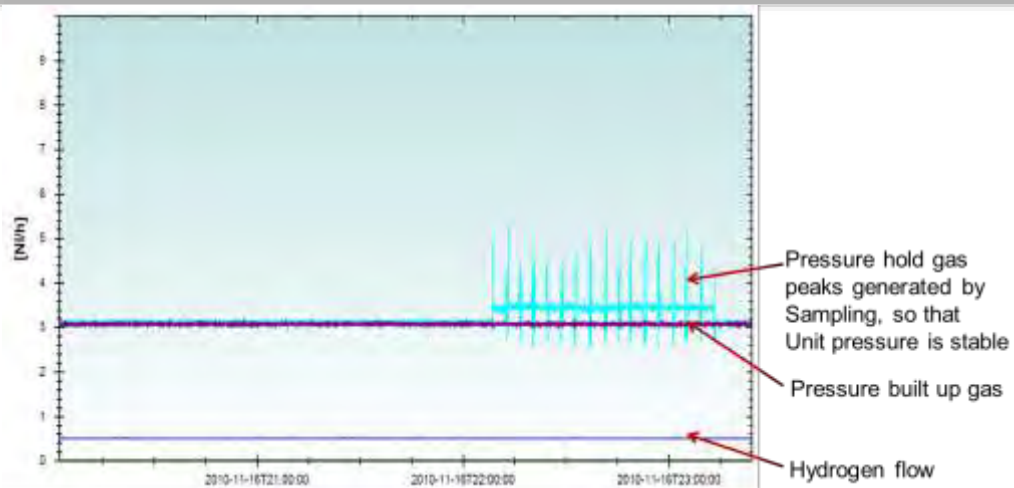
# Reactor Validation



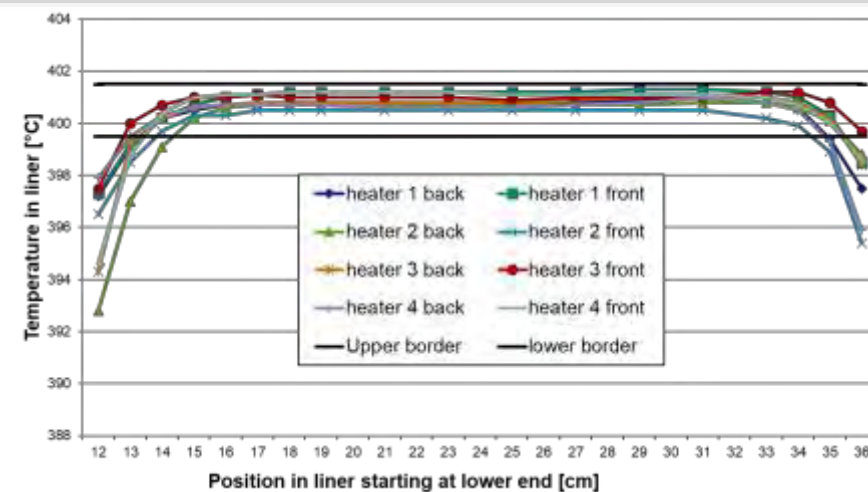
Process control softwares hteControl4 and Zenon



Pressure stability at 100barg



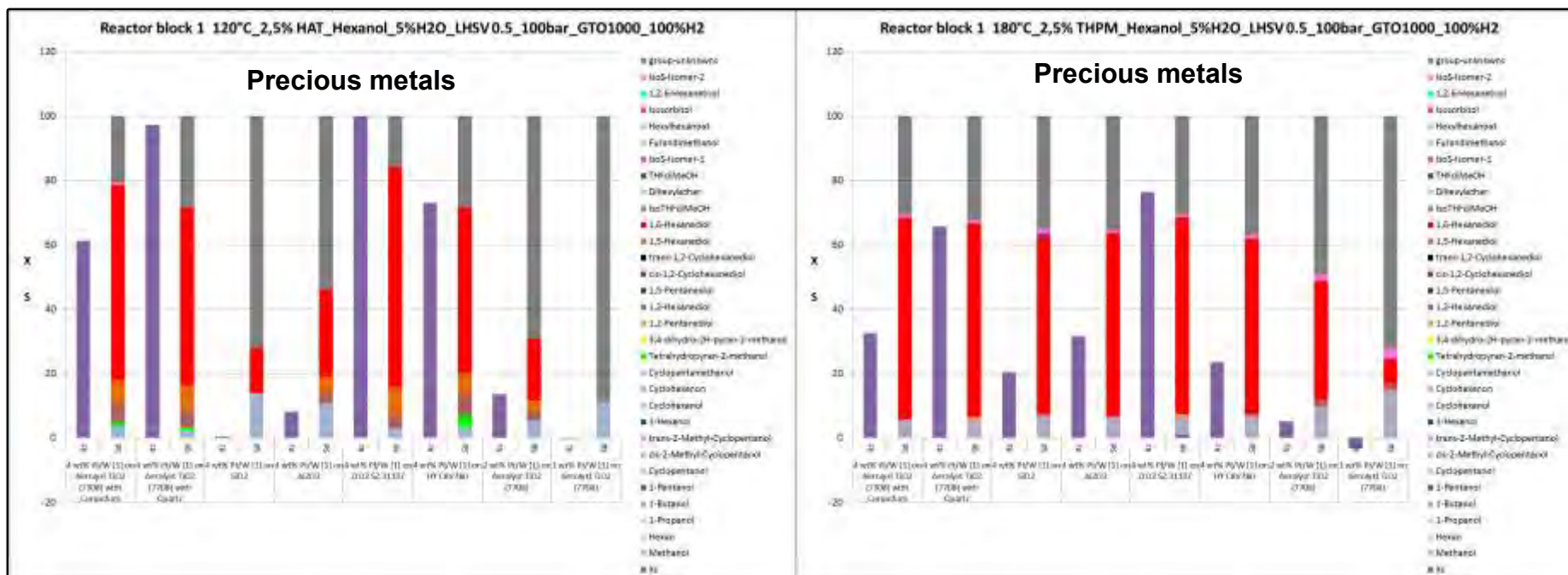
Flow stability at 100barg



Isothermal temperature profile for catalyst bed zone ( $\pm 1$  °C)

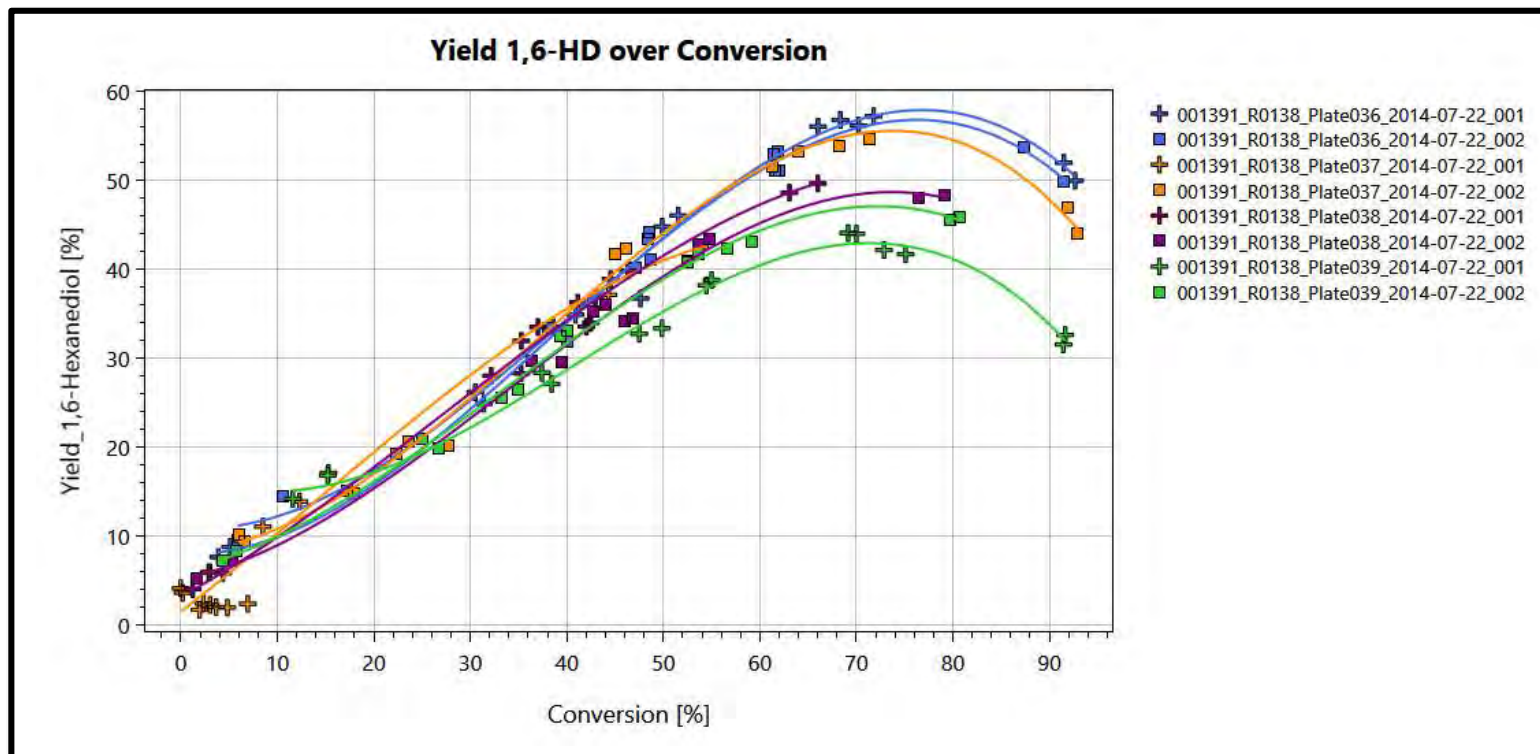


# High Throughput Screening



- Tested approximately 500 catalysts, 16 catalysts at a time, catalyst loading 1.5 ml
- Compared **base and precious metal catalysts**
- Screened **different substrates** (1,2,6-HAT, THP2M, THFDM, and others) to **1,6-Hexanediol**
- Screened **different solvent and/or solvent blends** (Water, Hexanol, Dioxane)
- Screened catalysts at **different temperatures** in parallel
- Continuous operation of up to **1 to 3 month(s) time on stream**
- Analytical identification of important unknowns by GC-MS

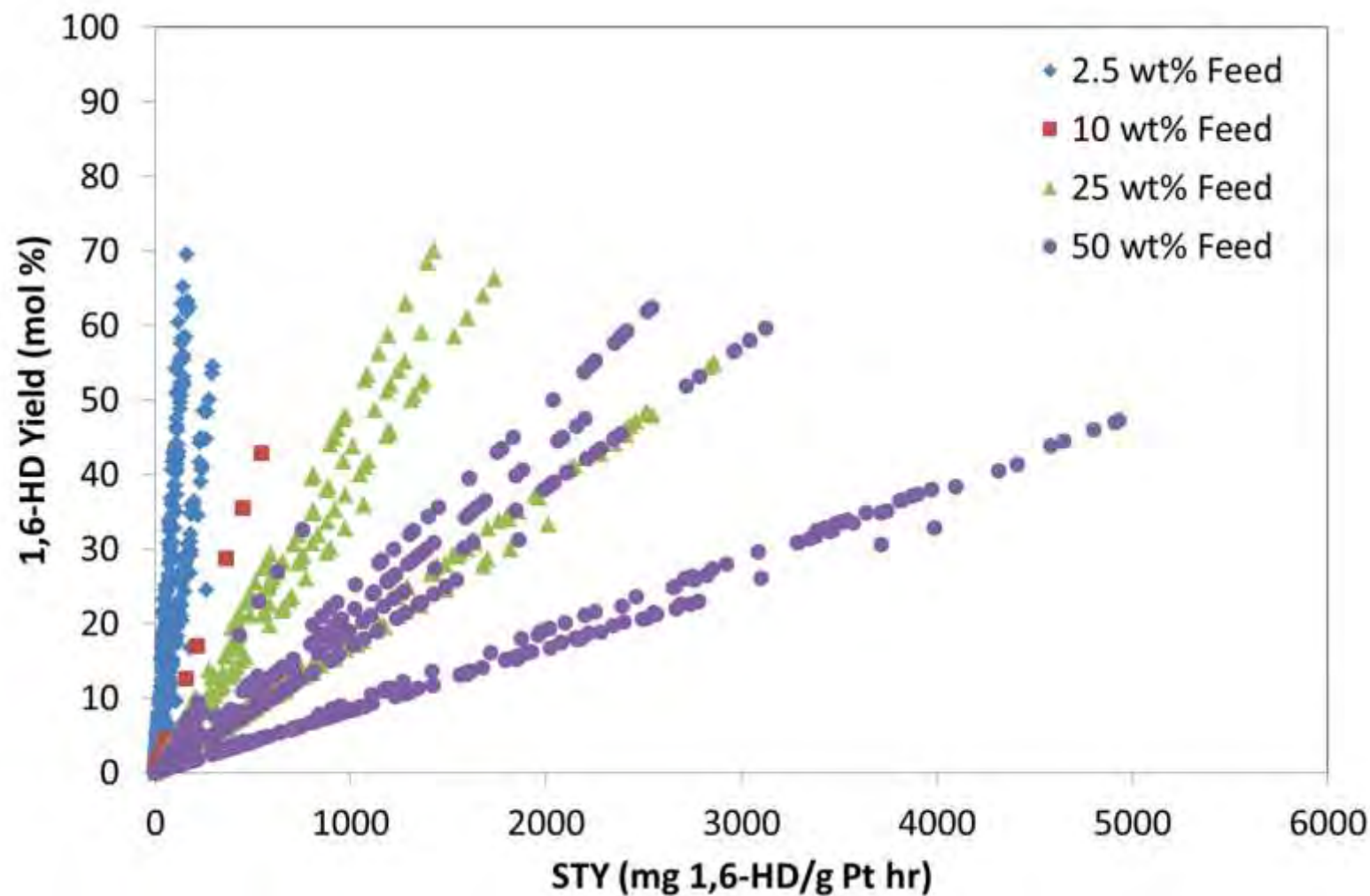
# Bench-scale Process Optimization



- Catalyst upscaling and **lead catalyst optimization**
- Individual **process optimization** of lead catalysts, catalyst loading 20 ml
  - Different Pressure and temperature range
  - Upflow vs. downflow reactor configuration
  - Per-pass conversion and recycle operation
- **Feedstock screening** for increased diversity
- 30 feed formulations (7 substrates, 3 solvents)
- 2 – 3 month time on stream (1000 – 2000 h TOS)

# Optimization of Pt/W Catalysts

## *STY as a Function of Metal Loading and Feed Composition*



# Summary

- Developed platform technology for selective hydrodeoxygenation of biomass
- Built biomass conversion catalysis and catalyst screening competency
- Identified proprietary classes of lead catalyst candidates enabling key functionalities in good yields (up to 85%) and selectivity
- Developed Supported Precious Metal Catalysts:
  - Pt/W/TiO<sub>2</sub>, Pt/WO<sub>3</sub>, Rh/Re/HY, Pt/Fe/TiO<sub>2</sub>
- Demonstrated the lead catalyst selection from batch screening of catalysts to continuous fixed bed reactor technology for the hydrodeoxygenation of critical renewable chemical precursors to 1,6-hexanediol
- Established sophisticated catalyst characterization tools; in conjunction with kinetic data, gaining detailed insight towards reaction mechanism and catalyst's structure activity relationships



# Change Takes Time

I am certain that one day we will be successful in changing hearts and minds. Perhaps the change will be slow. Perhaps it will come one day at a time and one person at a time. But one day, we'll find that whole nations have changed, and our world has embraced a new paradigm and we will have a blueprint for safe and sustainable products and processes, by design, for our future generations.



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